**Amendments to the Claims**

1. (Previously presented) A composition comprising
an ethylene-propylene-diene rubber component; and,
a process oil having a kinematic viscosity at 100 °C greater than 8 cSt and a pour point of below 10°C wherein the process oil is obtained by a process comprising:
(a) hydrocracking/hydroisomerizing a feed comprising a Fischer-Tropsch synthesis product;
(b) isolating from the product of step (a) a process oil precursor fraction; and,
(c) dewaxing the process oil precursor fraction obtained in step (b) to obtain the process oil.

2. (Previously presented) The composition of claim 1, wherein the process oil has a flash point of above 260 °C according to ISO 2592.

3. (Previously presented) The composition of claim 1, wherein the UV adsorption of the process oil at 300 nm is less than 0.6% according to ASTM D 2008-A1.

4. (Canceled).

5. (Currently amended) The composition of claim 1, wherein the kinematic viscosity at 100 °C is greater than 9 cSt.

6. (Previously presented) The composition of claim 1, wherein step (c) is performed by solvent dewaxing.

7. (Previously presented) The composition of claim 1, wherein step (c) is performed by catalytic dewaxing.

8. (Currently amended) The composition of claim 1, wherein the conversion in step (a) is between 25 and 65 wt%, based on the weight percentage of the feed boiling above 370 °C which reacts per pass to a fraction boiling below 370 °C.

9. (Previously presented) The composition of claim 1, wherein the composition furthermore comprises a poly-olefin component.

10. (Previously presented) The composition of claim 9, wherein the poly-olefin is polypropylene.

11. (New) The composition of claim 1 wherein (c) further comprises separating a lower boiling fraction from the dewaxed product to produce the process oil.

12. (New) A composition comprising

an ethylene-propylene-diene rubber component;

polypropylene; and,

a process oil having a kinematic viscosity at 100 °C greater than 8 cSt and a pour point of below 10°C wherein the process oil is obtained by a process comprising:

(a) hydrocracking/hydroisomerizing a feed comprising a Fischer-Tropsch synthesis product;

(b) isolating from the product of step (a) a process oil precursor fraction; and,

(c) solvent dewaxing the process oil precursor fraction obtained in step (b) to obtain the process oil.

13. (New) The composition of claim 12, wherein the kinematic viscosity at 100 °C is greater than 9 cSt.

14. (New) A composition comprising

an ethylene-propylene-diene rubber component; and,

a process oil having a kinematic viscosity at 100 °C greater than 8 cSt, a pour point of below 10°C, and an evaporation loss at 107 °C during 22 hours of less than 0.05 wt% according to ASTM D 972, wherein the process oil is obtained by a process comprising:

(a) hydrocracking/hydroisomerizing a feed comprising a Fischer-Tropsch synthesis product;

(b) isolating from the product of step (a) a process oil precursor fraction; and,

(c) dewaxing the process oil precursor fraction obtained in step (b) to obtain the process oil.

point of above 260 °C according to ISO 2592.

16. (New) The composition of claim 15, wherein the UV adsorption of the process oil at 300 nm is less than 0.6% according to ASTM D 2008-A1.

17. (New) The composition of claim 16, wherein the kinematic viscosity at 100 °C is greater than 9 cSt.

18. (New) The composition of claim 17, wherein step (c) is performed by solvent dewaxing.

19. (New) The composition of claim 17, wherein step (c) is performed by catalytic dewaxing.

20. (New) The composition of claim 19, wherein the conversion in step (a) is between 25 and 65 wt%, based on the weight percentage of the feed boiling above 370 °C which reacts per pass to a fraction boiling below 370 °C.

21. (New) The composition of claim 20, wherein the composition furthermore comprises a poly-olefin component.

22. (New) The composition of claim 21, wherein the poly-olefin is polypropylene.

23. (New) The composition of claim 22 wherein (c) further comprises separating a lower boiling fraction from the dewaxed product to produce the process oil.